## **Biosolids Gasification A Technology Review**

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### **Gasification - Outline**

- Background
- Process
  - Reactions/Equations
- Technologies
- What's Been or Being Done for Biosolids

## **Gasification Background**

- Charcoal Formation
  - (Pyrolysis first stage of gasification)
  - Several thousand years old
- Gasification
  - Large scale use on coal
  - 19<sup>th</sup> century
  - Used today for coal, wood, ag waste and many other materials

#### **Gasification - Process**

### **Steps in Gasification Process**

- Pyrolysis (Volatilization)
  - Release volatile compounds produce char (carbon solids)
  - Occurs at about 400°C to 700°C
- Combustion (Oxidation)
  - Combust char to create heat for process
  - Can be skipped if and external heat source used
- Gasification (Reduction)
  - Produce Synthesis gas
  - Occurs at about 850°C to 1,200°C

#### **Gasification - Reactions**

#### Combustion (Oxidation) Reactions

$$C + \frac{1}{2}O_2 \rightarrow CO$$

(- 111MJ/Kmol)

$$CO + \frac{1}{2}O_2 \rightarrow CO_2$$
 (- 283 MJ/Kmol)

$$H_2 + \frac{1}{2} O_2 \rightarrow H_2 O$$

(- 242 MJ/Kmol)

#### **Boudouard Reaction**

$$C + CO_2 \iff 2CO$$

(+ 172 MJ/Kmol)

#### Water Gas Reaction

$$C + H_2O \implies CO + H_2$$

(+ 131 MJ/Kmol)

#### Methane Formation

$$C + 2H_2 \longrightarrow CH_4$$

(- 75 MJ/Kmol)

#### CO Shift Reaction

$$CO + H_2O \longrightarrow CO_2 + H_2$$
 (- 41 MJ/Kmol)

#### Steam Methane Reforming Reaction

$$CH_4 + H_2O \longrightarrow CO + 3H_2$$
 (+ 206 MJ/Kmol)

Ref: Higman, Christopher, Van Der Burgt, Maarten, Gasification, Second Edition, 2008

## **Gasification - Technologies**

### Reactor Types

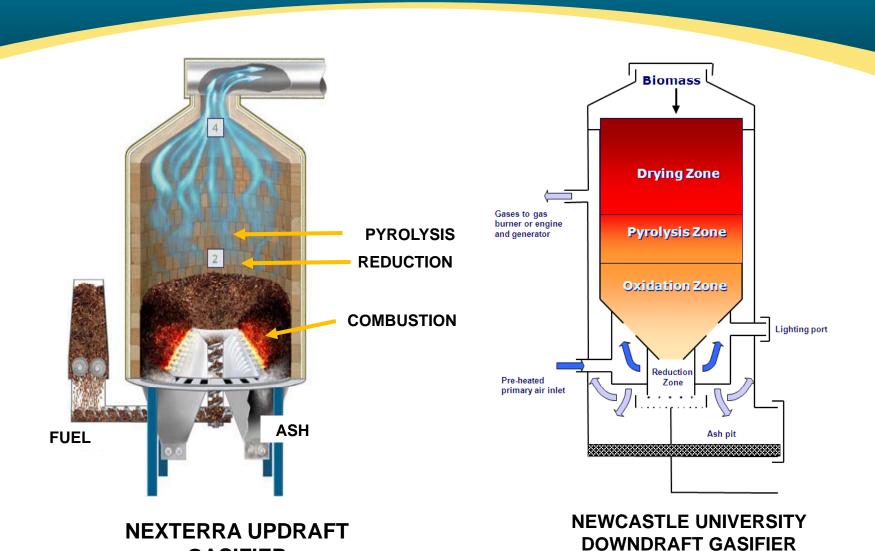
- Fixed Bed Updraft (Countercurrent)
- Fixed Bed Downdraft (Co-Current)
- Fluidized Bed
- Entrained Flow

### **Heating Methods**

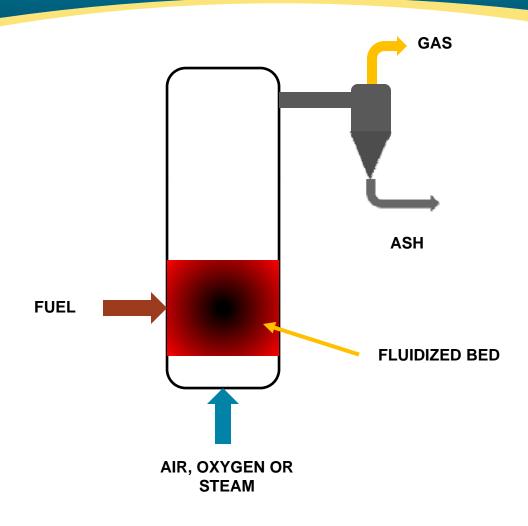
- Fuel/Char (Biomass or Biosolids)
- Plasma Torch
- Induction Heater

## **Technologies –Fixed Bed Gasifiers**

**GASIFIER** 

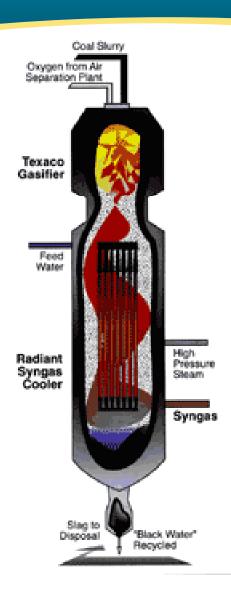


## **Technologies - Fluidized Bed Gasifier**



**Bubbling Fluidized Bed Gasifier** 

## **Technologies - Entrained Flow Gasifier**



## **Biosolids Experience - Ecotech**

#### **EcoTech Gasification**

Location:

Started Operation:

Current Status:

• Technology:

• Equipment Supplier:

• Size:

Philadelphia, PA

June 2005

Out of operations

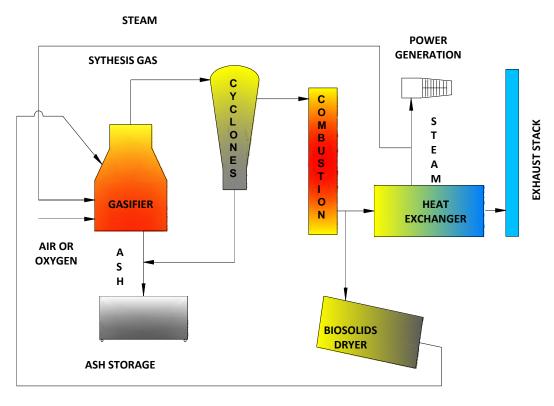
Downdraft Fixed Bed

Primenergy

10 Wet tons per hour



## **Biosolids Experience - Ecotech**



**DRIED BIOSOLIDS** 

## **Biosolids Experience - Ecotech**

#### Issues

- Inconstant energy content
- Both water and wastewater sludge
- Digestion of wastewater sludge reduced btu value
- Ferric Chloride added to particulate and slag production
- Horizontal heat exchanger slag did not drain well hardened (cleaning every 2 weeks)

#### MaxWest

• Location: Sanford, FL

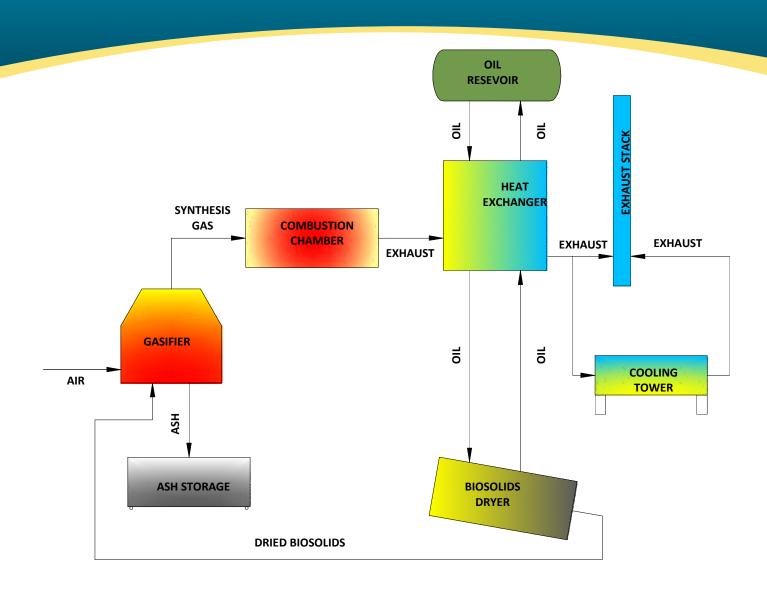
Started operation: Fall 2009

Current status: Operating

Technology: Downdraft Fixed Bed

• Size: 720 to 1,140 lbs/hr dried biosolids (85% to 92%)





#### General

- Product Hot exhaust provides heat to run the dryer
- Immediate high temp combustion of gas no gas cleaning needed
- The system is a closed loop disposal technology
- No power production
- Limited emissions information
- Odor from fuel loading and ash unloading easily solved
- MaxWest operates the dewatering, drying and gasification

#### Economics - Sanford, FL

- Flat fee per month (\$21,572/month)
- 3% annual increase (+\$647/month)
- Minimum required heat value 4,225 btu/lbs delivered
- MaxWest to deliver hot oil to dryer
  - In reality MaxWest is operating dryer and dewatering
- Revenue sharing for outside feedstocks

## Biosolids Experience – Kopf Pilot

#### Kopf

• Location: Balingen, Germany

• Started Operation: 2006

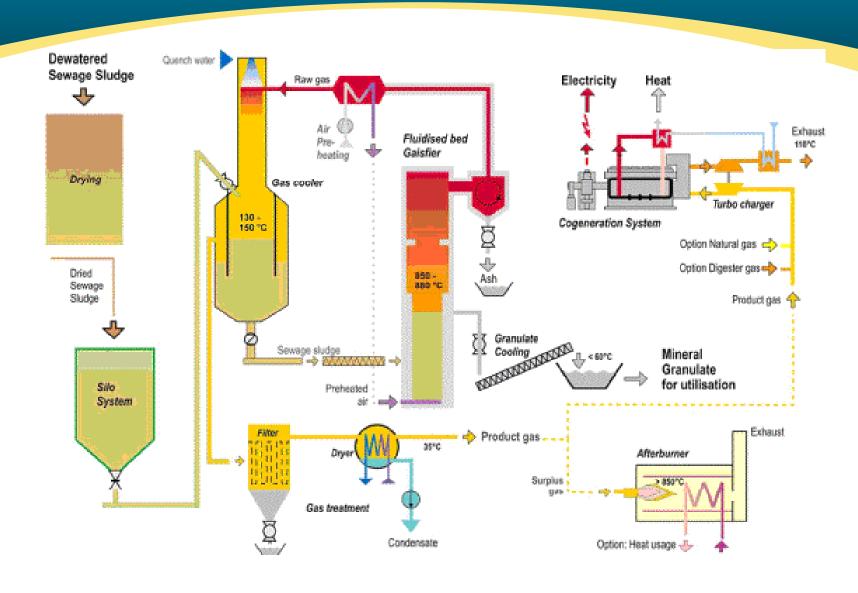
Current status: Operating

Technology: Fluidized Bed Gasifier

• Size: 331 lbs/hr



## Biosolids Experience – Kopf



## Biosolids Experience – Kopf Pilot

#### General

- Biosolids dried separately
  - Dried to 85% solids
- Gas used in CHP
- Reported output 70 kw of electricity
  - 15 kw to run process
  - 55 kw available for power generation

## Biosolids Experience – Waste to Energy Ltd

#### Waste to Energy Ltd Pilot

Location: Anglican Water Wellingborough, England

• Started operation 2005

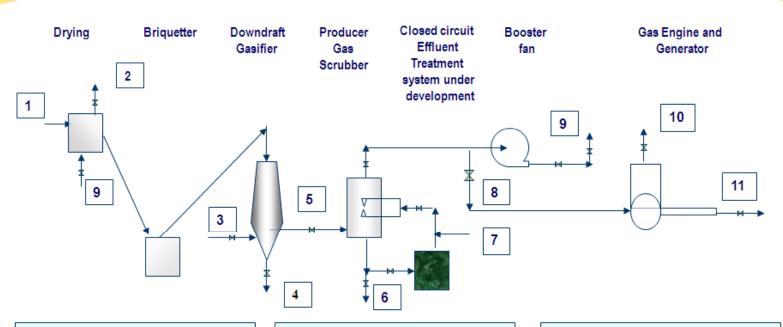
Current Status Unknown

Technology: Downdraft Fixed Bed Gasifier (mobile skid)

mounted unit)

• Size: 275 lbs/hr

## Biosolids Experience – Waste to Energy Ltd



- 1- After centrifuge sludge enters into the dryer at 20-25% ds
- 2- Clean dust free exhaust gases after scrubber
- 3- Air enters the gasifier at about stoichiometric levels
- 4- White ash (low carbon) with leachable metals but when used as road aggregate, produce zero leacheate.
- 5- Hot producer gas at ~400°C exits the reduction zone in the gasifier and enters the scrubber where it is quenched to ~50°C thereby removing dust, acid gases, tars and also eliminate dioxin reformation.
- 6- Scrubber residue Tars, dust
- 7- Make up water

- 8- Clean producer gas mainly consisting of H<sub>2</sub>, CO, CH<sub>4</sub>, CO<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, to duel fuel compression engine
- 9- Clean gas to dryer or invisible flare

#### Tokyo Bureau of Sewerage

• Location: Tokyo

• Started operations: 2005

• Current status: Ceased operation in 2006 (3,400 hours of

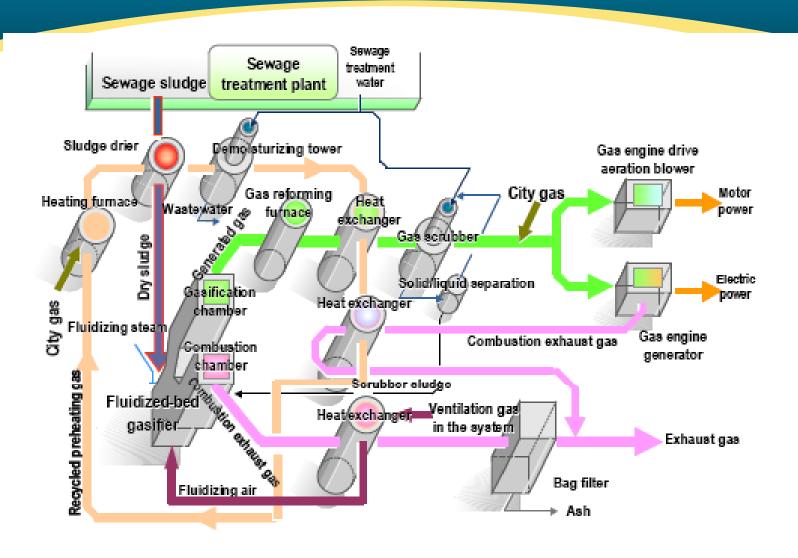
operation)

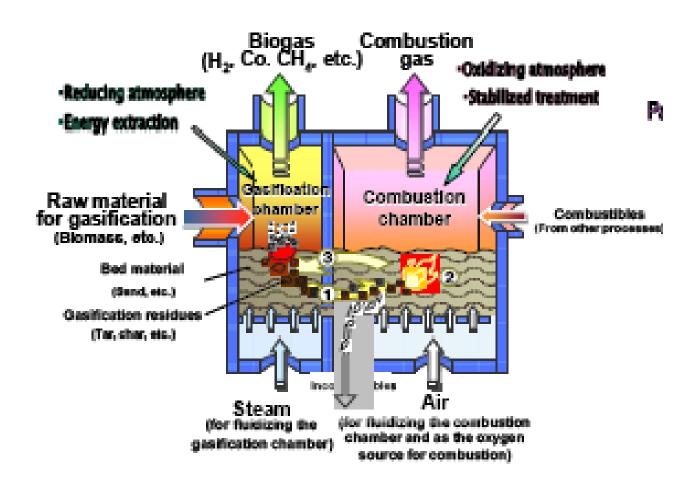
Technology: Internal Circulating Fluidized Bed

• Size 1,375 lbs per hour

Reference: Takahashi, Hajime, "Study on Sewage Sludge Gasification", Bureau of Sewerage, Tokyo Metropolitan Government







#### Results

- Used a blend of 55% syn gas and 45% natural gas
- Power output 200 kw
- Sludge drying included in output
- Steam generation included in output
- 55% reduction in GHG emission over incineration
- 19% reduction in purchased energy over incineration

## **Biosolids Experience - Pyromex**

### Pyromex Pilot

• Location: Emmerich, Germany

• Started operation: 2000

• Current status: Ceased 2003 equipment moved to commercial

client

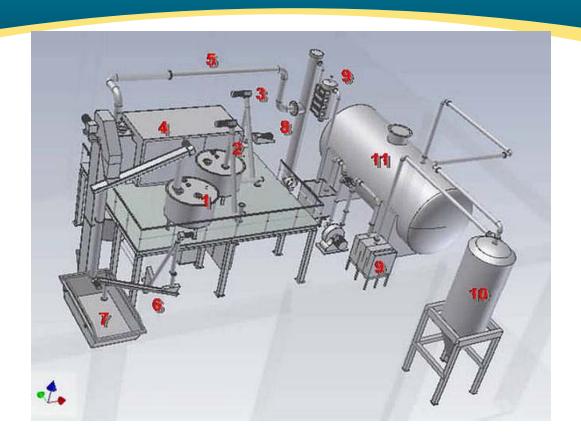
Technology: Induction heated rotating gasifier

• Size: 2,290 lbs/hr





## **Biosolids Experience - Pyromex**



- 1 Input material storage tanks
- 2 Rotation valves
- 3 Feed auger
- 4 Reactor

- 5 Syngas pipe
- 6 Inert residue outfeed
- 7 Inert residue silo
- 8 Sedimentation

- 9 Scrubber
- 10 Cyclone
- 11 Cleaned syngas to gas

## **Biosolids Experience - Pyromex**

#### Results

- Sludge dried to 85% solids
- High temperature process 1,750°C
- Reported Energy Output

Energy retrieved
 1035 kwh/tonne sludge

Gasifier energy consumption 345 kwh/tonne

Sludge dryer power demand
 540 kwh/tonne

External heating means no combustion of char/feedstock

#### **Conclusions**

- If drying included gasification is a closed loop disposal technology
- If digester gas used for drying energy production is possible
- Avoiding steam simplifies process but reduces energy output
- Direct burning of syn gas avoids gas cleaning, simplifies the process reduces options for end uses

## Questions

